## DOWNTOWN KODIAK SEWER MAIN \& LIFT STATION 2 FORCE MAIN PIPE EVALUATION

EXISTING GRAVITY MAIN CAPACITY LOWER MILL BAY TO MARINE WAY EAST
POSSIBLE UPSIZING OF THE MAIN FROM LOWER MILL BAY TO MARINE WAY EAST
EXISTING GRAVITY MAIN CAPACITY FROM OVERFLOW TO MARINE WAY WEST

## DOWNTOWN KODIAK SEWER MAIN \& LIFT STATION 2 FORCE MAIN PIPE EVALUATION

EXISTING GRAVITY MAIN CAPACITY FROM REZANOF TO LIFT STATION 2 - MARINE WAY WEST

PROPOSED LIFT STATION 2 FORCE MAIN - MARINE WAY EAST (WITH 4-INCH OVERFLOW)

| Diameter (Inches) | Pipe Type <br> Class / SDR | Discharge <br> (GPM) | Pipe Inside <br> Diameter <br> (Inches) | Flow Velocity <br> (FPS) | Pipe Length <br> (Feet) | Hazen Williams <br> C-Factor | Frictional Head <br> Loss (Feet) | Total Dynamic <br> Head <br> (Feet) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 8 (Existing) | DIP CL52 | 800 | 8.390 | 4.64 | 550 | 130 | 5.37 | 24.69 |
| 8 | HDPE SDR21 | 800 | 7.754 | 5.44 | 550 | 140 | 6.87 | 26.19 |
| 8 | HDPE SDR17 | 800 | 7.550 | 5.73 | 550 | 140 | 7.82 | 27.14 |
| 8 | HDPE SDR11 | 800 | 6.963 | 6.74 | 550 | 140 | 11.60 | 30 |
| 10 | HDPE SDR21 | 800 | 9.665 | 3.50 | 550 | 140 | 2.35 | 21.67 |
| 10 | HDPE SDR17 | 800 | 9.410 | 3.69 | 550 | 140 | 2.68 | 22.00 |
| 10 | HDPE SDR11 | 800 | 8.679 | 4.34 | 550 | 140 | 2.97 | 23.29 |

PROPOSED LIFT STATION 2 FORCE MAIN - MARINE WAY EAST (WITH 6-INCH OVERFLOW)
Static Head = 19.32

| Diameter (Inches) | Pipe Type <br> Class / SDR | Discharge (GPM) | Pipe Inside Diameter (Inches) | Flow Velocity (FPS) | Pipe Length (Feet) | Hazen Williams C-Factor | Frictional Head Loss (Feet) | Total Dynamic <br> Head <br> (Feet) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 8 | DIP CL52 | 1,300 | 8.390 | 7.54 | 550 | 130 | 13.20 | 32.52 |
| 12 | DIP CL52 | 1,300 | 12.450 | 3.43 | 550 | 140 | 1.69 | 21.01 |
| 12 | HDPE SDR21 | 1,300 | 11.463 | 4.04 | 550 | 140 | 2.52 | 21.84 |
| 12 | HDPE SDR17 | 1,300 | 11.160 | 4.26 | 550 | 140 | 2.87 | 22.19 |
| 12 | HDPE SDR11 | 1,300 | 10.293 | 5.01 | 550 | 140 | 4.26 | 23.58 |
| 14 | HDPE SDR21 | 1,300 | 11.301 | 4.16 | 550 | 140 | 2.70 | 22.02 |
| 14 | HDPE SDR17 | 1,300 | 12.253 | 3.54 | 550 | 140 | 1.82 | 21.14 |
| 14 | HDPE SDR11 | 1,300 | 12.586 | 3.35 | 550 | 140 | 1.60 | 20.92 |


| AC Pipe Inside Diameters |  |  |  |
| :---: | :---: | :---: | :---: |
| Nominal | Class 100 | Class 150 | Class 200 |
| 4 | 4.00 | 4.00 | 4.00 |
| 6 | 6.00 | 5.85 | 5.70 |
| 8 | 8.00 | 7.85 | 7.60 |
| 10 | 10.00 | 10.00 | 9.63 |
| 12 | 12.00 | 12.00 | 11.56 |
| 14 | 13.59 | 14.00 | 13.59 |
| 16 | 15.50 | 16.00 | 15.50 |

## MANNING'S FORMULA


$\mathrm{Q}=$ Discharge (cu. ft./sec.)
A = Cross-sectional Area of Flow (sq. ft.)
$\mathrm{n}=$ Coefficient of Roughness
R = Hydraulic Radius (ft.)
$\mathrm{S}=$ Slope of Pipe ( $\mathrm{ft} . / \mathrm{ft}$.)
Hydraulic Radius
$R=A / P$
A = Cross-sectional Area of Flow (sq. ft.)
P = Wetted perimeter (ft.)

Partially Full Pipe Flow Calculations - U.S. Units
I. Calculation of Discharge, Q, and average velocity, V
for pipes less than half full
Instructions: Enter values in blue boxes. Spreadsheet calculates values in yellow boxes

| Inputs |  | in | Calculations |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Pipe Diameter, $\mathbf{D}=$ | 12 |  | Pipe Diameter, $\mathbf{D}=$ | 1 | $f t$ |
| Depth of flow, $\mathbf{y}=$ (must have $\mathrm{y} \leq \mathrm{D} / 2$ ) | 4.8 | in | Pipe Radius, $\mathbf{r}=$ | 0.5 | ft |
|  |  |  | Circ. Segment Height, $\mathbf{h}=$ | 0.4 | ft |
| Manning |  |  |  |  |  |
| roughness, $\mathbf{n}_{\text {full }}=$ | 0.012 |  | Central Angle, $\boldsymbol{\theta}=$ | 2.74 | radians |
| Channel bottom |  | $\mathrm{ft} / \mathrm{ft}$ | Cross-Sect. Area, $\mathbf{A}=$ | 0.29 | $\mathrm{ft}^{2}$ |
| slope, $\mathbf{S}=$ | 0.0039 |  |  |  |  |
|  |  |  | Wetted Perimeter, $\mathbf{P}=$ | 1.4 | ft |
| y/D $=$ | 0.400 |  | Hydraulic Radius, $\mathbf{R}=$ | 0.21 | ft |
| $n / n_{\text {full }}=$ | 1.27 |  | Discharge, $\mathbf{Q}=$ | 0.641 | cfs |
| $\mathrm{n}=$ | 0.015 |  | Ave. Velocity, $\mathbf{V}=$ | 2.19 | $\mathrm{ft} / \mathrm{sec}$ |
|  |  |  | pipe \% full $\left[\left(A / A A_{\text {til }}\right) *\right.$ 100\%] $=$ | 37.35\% |  |

## Calculations

| If $0<y / D \leq 0.03$, then $\mathrm{n} / \mathrm{n}_{\text {full }}=$ | 2.33 |
| :---: | :---: |
| If $0.03<\mathrm{y} / \mathrm{D} \leq 0.1$, then $\mathrm{n} / \mathrm{n}_{\text {tull }}=$ | 1.73 |
| If $0.1<y / D \leq 0.2$, then $\mathrm{n} / \mathrm{n}_{\text {full }}=$ | 1.40 |
| If $0.2<y / D \leq 0.3$, then $\mathrm{n} / \mathrm{n}_{\text {tull }}=$ | 1.29 |
| If $0.3<\mathrm{y} / \mathrm{D} \leq 0.5$, then $\mathrm{n} / \mathrm{n}_{\text {tull }}=$ | 1.27 |

## Equations used for calculations:

$$
\begin{aligned}
& r=D / 2 \\
& h=y
\end{aligned}
$$

$$
\theta=2 \arccos \left(\frac{\mathrm{r}-\mathrm{h}}{\mathrm{r}}\right)
$$

$$
\mathrm{A}=\frac{\mathrm{r}^{2}(\theta-\sin \theta)}{2}
$$

$$
\mathrm{P}=\mathrm{r} * \theta
$$


$R=A / P \quad$ (hydraulic radius)
$\mathrm{Q}=(1.49 / \mathrm{n})(\mathrm{A})\left(\mathrm{R}^{2 / 3}\right)\left(\mathrm{S}^{1 / 2}\right) \quad$ (Manning Equation)
$V=Q / A$
287.30

| Equations used to calculate $\mathbf{n} / \mathbf{n}_{\text {full }}$ : |  |  |
| :---: | :---: | :---: |
| $0<y / D \leq 0.03$ | $n / n_{\text {fill }}=$ | $1+(y / D)(1 / 0.3)$ |
| $0.03<y / D \leq 0.1$ | $n / n_{\text {fll }}=$ | $1.1+(y / D-0.03)(12 / 7)$ |
| $0.1<\mathrm{y} / \mathrm{D} \leq 0.2$ | $n / n_{\text {tul }}=$ | $1.22+(y / D-0.1)(0.6)$ |
| $0.2<y / D \leq 0.3$ | $n / n_{\text {fill }}=$ | 1.29 |
| $0.3<y / D \leq 0.5$ | $n / n_{\text {fill }}=$ | $1.29-(y / D-0.3)(0.2)$ |



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Partially Full Pipe Flow Calculations - U.S. Units
II. Calculation of Discharge, Q, and average velocity, V
for pipes more than half full


Equation used for $n / n_{\text {full }}: n / n_{\text {tull }}=\mathbf{1 . 2 5}$ - (yID -0.5)*0.5 (for $\left.0.5 \leq y / D \leq 1\right)$

## Equations used for calculations:

$$
\begin{aligned}
& \mathrm{h}=2 \mathrm{r}-\mathrm{y} \\
& \theta=2 \arccos \left(\frac{\mathrm{r}-\mathrm{h}}{\mathrm{r}}\right) \\
& \mathrm{A}=\pi \mathrm{r}^{2}-\frac{\mathrm{r}^{2}(\theta-\sin \theta)}{2} \\
& \mathrm{P}=2 \pi \mathrm{r}-\mathrm{r}^{*} \theta \\
& \mathrm{R}=\mathrm{A} / \mathrm{P} \\
& \mathrm{Q}=(1.49 / \mathrm{n})(\mathrm{A})\left(\mathrm{R}^{2 / 3}\right)\left(\mathrm{S}^{1 / 2}\right) \quad \text { (Manning Equation) } \\
& \mathrm{V}=\mathrm{Q} / \mathrm{A} \\
& \text { (hydraulic radius) } \\
& \text { 962.1466248 }
\end{aligned}
$$



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Partially Full Pipe Flow Calculations - U.S. Units
III. Calculation of Normal Depth for Pipes Less Than Half Full
Instructions: Enter values in blue boxes. Spreadsheet calculates values in yellow boxes

| Inputs |  |  |
| :---: | :---: | :---: |
| Pipe Diameter, $\mathbf{D}=$ | 8.5 | in |
| Manning roughness, $\mathbf{n}_{\text {full }}=$ | 0.013 |  |
| Channel bottom slope, $\mathbf{S}=$ | 0.0072 | $\mathrm{ft} / \mathrm{ft}$ |
| Volumetric Flow Rate, $\mathbf{Q}=$ | 1 | cfs |
| Iterative (trial \& error) Solution: |  |  |
| (Select values of $y_{0}$, to find the value of $y_{0}$ that makes $\left(A^{*} \mathrm{R}^{2 / 3}\right) / n$ as close to the target value as possible) |  |  |


| Calculations | $\mathrm{h}=\mathrm{y}$ |  |
| :--- | :--- | :--- |
| Pipe Diameter, $\mathrm{D}=0.708333$ | ft | $\theta=2 \arccos \left(\frac{\mathrm{r}-\mathrm{h}}{\mathrm{r}}\right)$ |
| Pipe radius, $\mathrm{r}=$ | 0.4 | ft |
| The Manning equation can be rearranged to: | $\mathrm{A}=\frac{\mathrm{r}^{2}(\theta-\sin \theta)}{2}$ |  |
|  | $\mathrm{P}=\mathrm{r}^{*} \theta$ |  |

$R=A / P$
(hydraulic radius)

$$
\begin{aligned}
& \mathrm{Q}=(1.49 / \mathrm{n})(\mathrm{A})\left(\mathrm{R}^{2 / 3}\right)\left(\mathrm{S}^{1 / 2}\right) \quad \text { (Manning Equation) } \\
& \mathrm{V}=\mathrm{Q} / \mathrm{A}
\end{aligned}
$$

## Partially Full Pipe Flow Calculations - U.S. Units

IV. Calculation of Normal Depth for Pipes More Than Half Full

Instructions: Enter values in blue boxes. Spreadsheet calculates values in yellow boxes


Volumetric Flow Rate, $\mathbf{Q}=\quad 18$ cfs

Iterative (trial \& error) Solution
(Select values of $y_{0}$, to find the value of $y_{0}$ that makes $\left(A^{\star} R^{2 / 3}\right) / n$ as close to the target value as possible)

| $\mathrm{y}_{0}, \mathrm{ft}$ | $\mathrm{h}, \mathrm{ft}$ | $\theta$, radians | $\mathrm{A}, \mathrm{ft}^{2}$ |
| :---: | :---: | :---: | :---: |
| 3 | 1.00 | 2.094 | 10.11 |
| 2 | 2.00 | 3.142 | 6.28 |
| 2.5 | 1.50 | 2.636 | 8.26 |
| 2.51 | 1.49 | 2.626 | 8.30 |
| 2.52 | 1.48 | 2.616 | 8.34 |
| 2.53 | 1.47 | 2.605 | 8.38 |

## $\mathrm{Q} /\left(1.49^{*} \mathrm{~S}^{1 / 2}\right)=\left(\mathrm{A}^{*} \mathrm{R}^{2 / 3}\right) / \mathrm{n}$

 for $\left(A^{*} \mathrm{R}^{2 / 3}\right) / n$
difference from

| $n$ | $\mathrm{P}, \mathrm{ft}$ | $\left(\mathrm{A}^{*} \mathrm{R}^{2 / 3}\right) / \mathrm{n}$ | target value |
| :---: | :---: | :---: | :---: |
| 0.0124 | 8.38 | 926.0 | 228.5 |
| 0.0138 | 6.28 | 457.0 | -240.5 |
| 0.0131 | 7.29 | 687.3 | -10.2 |
| 0.0130 | 7.31 | 692.1 | -5.4 |
| 0.0130 | 7.34 | 696.9 | -0.6 |
| 0.0130 | 7.36 | 701.7 | 4.2 |

Equations used for calculations:
$r=D / 2$
$h=2 r-y$
$\theta=2 \arccos \left(\frac{\mathrm{r}-\mathrm{h}}{\mathrm{r}}\right)$
$\mathrm{A}=\pi \mathrm{r}^{2}-\frac{\mathrm{r}^{2}(\theta-\sin \theta)}{2}$
$\mathrm{P}=2 \pi \mathrm{r}-\mathrm{r}^{*} \theta$


Partially Full Pipe Flow Parameters (More Than Half Full)

$$
\mathrm{R}=\mathrm{A} / \mathrm{P} \quad \text { (hydraulic radius) }
$$

$$
\mathrm{Q}=(1.49 / n)(A)\left(\mathrm{R}^{2 / 3}\right)\left(\mathrm{S}^{1 / 2}\right) \quad \text { (Manning Equation) }
$$

$$
\mathrm{V}=\mathrm{Q} / \mathrm{A}
$$

NOTE: For $\mathrm{Q}=18 \mathrm{cfs}$, this set of calculations shows that $\mathrm{y}_{0}=2.52 \mathrm{ft}$
(accurate to 3 significant figures)

NOTE: For $0.5 \leq y / D \leq 1: n / n_{\text {full }}=1.25-(y / D-0.5)^{*} 0.5$ (see graph below)


